

EFFECT OF COAGULATION BATH TEMPERATURE TO
THE STRUCTURE AND MEMBRANE SEPARATION
PERFORMANCE.

WILLIBORD PETER

L
44
FST
21
2005

FAKULTI SAINS DAN TEKNOLOGI
LEJ UNIVERSITI SAINS DAN TEKNOLOGI MALAYSIA

2005

UN:4698

EFFECT OF COAGULATION BATH TEMPERATURE TO THE STRUCTURE
AND MEMBRANE SEPARATION PERFORMANCE.

Willibrord Peter

Research Report submitted in partial fulfillment of
The requirements for the degree of
Bachelor of Technology (Environmental)

Department of Engineering Science
Faculty of Science and Technology
KOLEJ UNIVERSITI SAINS DAN TEKNOLOGI MALAYSIA
2005

Lp
45
FST
5
2005

"

1100036927



JABATAN SAINS KEJURUTERAAN
FAKULTI SAINS DAN TEKNOLOGI
KOLEJ UNIVERSITI SAINS DAN TEKNOLOGI MALAYSIA

PENGAKUAN DAN PENGESAHAN LAPORAN
PROJEK PENYELIDIKAN I DAN II

Adalah ini diakui dan disahkan bahawa laporan penyelidikan bertajuk:

THE EFFECT OF COAGULATION BATH TEMPERATURE TO THE
MEMBRANE STRUCTURE AND PERFORMANCE

oleh Willibrord Peter, No. Matrik UK 7366 telah diperiksa dan semua pembetulan yang disarankan telah dilakukan. Laporan ini dikemukakan kepada Jabatan Sains Kejuruteraan sebagai memenuhi sebahagian daripada keperluan memperolehi Ijazah Sarjana Muda Teknologi (Alam Sekitar), Fakulti Sains dan Teknologi, Kolej Universiti Sains dan Teknologi Malaysia.

Disahkan oleh:

Penyelia Utama

DR. NORA'AINI BINTI ALI

Nama:

Pensyarah

Jabatan Sains Kejuruteraan

Fakulti Sains dan Teknologi

Cop Rasmi:

Kolej Universiti Sains dan Teknologi Malaysia
21030 Kuala Terengganu.

Tarikh: 20.4.05

Penyelia Kedua (jika ada)

ASMAIDI BIN ALI @ MAHMUD

Nama:

Pensyarah

Jabatan Sains Kejuruteraan

Fakulti Sains dan Teknologi

Cop Rasmi:

Kolej Universiti Sains dan Teknologi Malaysia
21030 Kuala Terengganu

Tarikh: 20.4.05

Ketua Jabatan Sains Kejuruteraan

Nama:

MUHAMMAD AHMAD JUSOH

Cop Rasmi:

Kolej Universiti Sains dan Teknologi Malaysia
21030 Kuala Terengganu

Tarikh: 21.4.05

ACKNOWLEDGEMENT

First and foremost, I would like to express my deepest gratitude to my supervisor, Dr. Nora'aini bte Ali and to En Zul, for all their guidance and support through out the finishing of my project. Their effort on teaching and giving information related to my study has helping me to do my study in a very confident ways.

In addition to that, I would like to thank to all the lectures especially my co-supervisor En. Asmadi Ali for all their advices and guidance. Not to forget all the staffs, especially En Razman, Cik Mazalina, En. Rozali and En. Mahmood for all the supports they gave through my lab works.

Last but not least, to all who have been involved in helping me with my project especially those who were under the same project as me and to all my friends, I would like to thank them for their helps and supports in my project lab and project paper.

LIST OF CONTENTS

| | |
|-----------------------------|-------------|
| FRONT COVER | i |
| THESIS APPROVAL FORM | ii |
| ACKNOWLEDGEMENTS | iii |
| LIST OF CONTENTS | iv |
| LIST OF TABLES | vii |
| LIST OF FIGURES | viii |
| ABBREVIATION/SYMBOLS | ix |
| LIST OF APPENDIXES | xi |
| ABSTRACT | xii |
| ABSTRAK | xiii |

CHAPTER 1 INTRODUCTION

| | | |
|-----|---------------------------------------|---|
| 1.1 | Definition of Membrane | 1 |
| 1.2 | Basic Principle of Membrane Processes | 2 |
| 1.3 | Membrane Development History | 4 |
| 1.4 | Problem Statement | 7 |
| 1.5 | Research Objective | 8 |
| 1.6 | Scope of Research | 9 |

CHAPTER 2 LITERATURE REVIEW

| | | |
|-------|---|----|
| 2.1 | Membrane And Its Application | 10 |
| 2.2 | Membrane Preparation | 11 |
| 2.3 | Asymmetric Membrane | 11 |
| 2.4 | Selection of Polymer-Solvent and Non-Solvent (Precipitant) System | 12 |
| 2.4.1 | Polyethersulfone | 14 |
| 2.4.2 | Solvent (N-methyl-2-pyrrolidone) | 14 |
| 2.4.3 | Non-solvent | 15 |
| 2.5 | Polymer Concentration | 15 |
| 2.6 | Effect of Internal Coagulant | 16 |
| 2.7 | Effect of Coagulation Bath (gelation media) Temperatures to the Membrane Flux and Rejections | 17 |
| 2.8 | Membrane Process Phase Inversion | 19 |
| 2.9 | Limitation of Membrane Processes | 21 |
| 2.9.1 | Concentration polarisation | 22 |
| 2.10 | Nanofiltration Membrane | 23 |

CHAPTER 3 METHODOLOGY

| | | |
|-------|--|----|
| 3.1 | Materials | 25 |
| 3.2 | Dope Preparation | 26 |
| 3.3 | Membrane Preparation | 27 |
| 3.4 | Preparation of Testing Solution (NaCl) | 28 |
| 3.4.1 | Dilution of Salt | 28 |
| 3.4.2 | Stock Solution Dilution | 29 |

| | | |
|-------------------|---|----|
| 3.4 | Membrane Testing (Performance Evaluation) | 29 |
| 3.6 | Membrane Characterization | 31 |
| | | |
| CHAPTER 4 | RESULTS AND DISCUSSIONS | |
| 4.1 | Mechanism of produced Membrane during Wet Phase Inversion | 39 |
| 4.2 | Pure water Flux and Sodium Chloride Rejection Measurement | 40 |
| 4.3 | The Effect of Coagulation Bath Temperature To The Membrane Permeability | 40 |
| 4.4 | Effect of Coagulation Bath Temperature to the Rejection of Sodium Chloride. | 44 |
| 4.5 | Rejection of Sodium Chloride as a Function of Applied Pressure. | 46 |
| 4.6 | Effect of Coagulation Bath Temperature to the Membrane Structures. | 49 |
| | | |
| CHAPTER 5 | CONCLUSION AND RECOMMENDATIONS | |
| 5.1 | Conclusion | 52 |
| 5.2 | Recommendations | 54 |
| | | |
| REFERENCES | | 55 |
| APPENDIX | | 59 |
| VITAE | | 68 |

LIST OF TABLE

| Table | | Page |
|--------------|---|-------------|
| 1.1 | Technical Development of Membranes | 7 |
| 3.1 | Summary for the Asymmetric Membrane Formation. | 28 |
| 3.2 | The solute radius and diffusivity of NaCl | 35 |
| 3.3 | The obtained values of diffusion coefficient for selected salt | 35 |
| 4.1 | Permeability of Membranes | 42 |
| 4.2 | Relation between permeability and rejection as a function of different Coagulation bath temperatures applied. | 45 |
| 4.3 | Relation between permeability, flux and rejection as function of different Coagulation bath temperatures applied. | 48 |

LIST OF FIGURES

| Figure | Page |
|--|-------------|
| 2.1 Molecular Chain of Polyethersulfone | 14 |
| 2.2 Chemical structure for NMP | 15 |
| 2.3 Schematic Drawing of Wet Phase Inversion | 21 |
| 3.1 Preparation of Casting Solution | 26 |
| 3.2 Membrane Casting Machine | 27 |
| 3.3 Formation of Membrane in Coagulation Bath | 27 |
| 3.4 Dead-End Filtration set up | 31 |
| 3.5 Scanning Electron Microscope | 36 |
| 3.6 flow chart indicating the whole methodology experimental unit | 37 |
| 4.1 Schematic Drawing of Non-Solvent/Solvent Exchange Process at the Coagulation Media/Polymer Solution Interface | 39 |
| 4.2 (a) Dependence of flux as a function of pressure for membrane coagulated at 27°. | 41 |
| 4.2 (b) Dependence of flux as a function of pressure for membrane coagulated at 5°. | 41 |
| 4.2 (c) Dependence of flux as a function of pressure for membrane coagulated at 50°. | 41 |
| 4.3 Dependence of NaCl rejection as a function of applied Pressure for membrane coagulated at 27°. | 44 |
| 4.4 The Dependence of Flux and Rejection as a Function of Applied Pressure | 47 |
| 4.5 Scanning electronic photomicrograph of membrane coagulated At different temperature: (a) PES-50°C, (b) PES-5°C,(c) PES-27°C. | |

ABBREVIATION/ SYMBOLS

| | | |
|----------------|---|---------------------------------------|
| DD | - | Diffusion Dialysis |
| DMAc | - | N,N-Dimethyl-Acetamide |
| ED | - | Electrodialysis |
| INOS | - | Institute Oceanography |
| MF | - | Microfiltration |
| ME | - | Membrane Electrolysis |
| Mol | - | Molar |
| mL | - | Millilitre |
| NF | - | Nanofiltration |
| NMP | - | N-Methyl-2-Pyrrolidone |
| Nm | - | Nanometer |
| NaCl | - | Natrium Chloride/Sodium Chloride |
| PVDF | - | Polyvinylidene Fluoride |
| PES | - | Polyethersulfone |
| RO | - | Reverse Osmosis |
| SEM | - | Scanning Electronic Microscope |
| UF | - | Ultrafiltration |
| A | - | Area of Membrane (m^2) |
| C _p | - | Concentration of Salt in the Permeate |
| C _f | - | Concentration of Salt in the Feed |

ABBREVIATION/SYMBOL

| | | |
|------------|---|--|
| G | - | Gram |
| Jv | - | Flux ($m^3/m^2 \text{ sec}$) |
| M | - | Wanted Molar of Salt |
| MW | - | Molecular Weight of Salt |
| M1 | - | Wanted Molar of salt Solution |
| M2 | - | Known Molar of Salt |
| Pm | - | Permeability of Membrane ($m^3/m^2 \text{ sec mPa}$) |
| ΔP | - | Applied Pressure (bar/Pa) |
| R(%) | - | Rejection Solute in Percentage |
| T | - | Time of Permeation Taken (sec) |
| V | - | Volume of salt Diluted in mL |
| V1 | - | Volume of Salt Solution |
| V2 | - | Volume of Salt Solution Need to be Pipette |
| v | - | Volume of Permeate(m^3) |
| Cb | - | Concentration of Salt in the Bulk |

APPENDIX

- A Preparation for Casting Solution of 100 mL
- B Preparation For Stock Solution of NaCl (0.1M)
- C Schematic Operational Principal for Stirred Cell
- D (a) Tables and Graphs For Permeability and Rejection for Membrane
Coagulated at 27°C.
- D (b) Tables and Graphs For Permeability and Rejection for Membrane
Coagulated at 5°C.
- D (c) Tables and Graphs For Permeability and Rejection for Membrane
Coagulated at 50°C.

ABSTRACT

The aim of this study was to investigate the effect of coagulation bath temperature to the membrane structure and performance. This parameter is important to be studied as the coagulation bath temperature effect directly to the separation performance and structure of membrane. Asymmetric flat sheet membrane were developed using a ternary system consisted of 21 polymer from Polyethersulfone, 72% solvent from N-methyl-2-pyrrolidone and 7% of water fabricated using electrically controlled semi-automated casting machine. The membrane cast was studied in different coagulation bath temperature of 5°C, 27°C and 50°C. The effect of the coagulation medium was measured in terms of pure water flux and rejections as a function of applied pressure to Natrium Chloride solution with concentration of 0.01 molar. The results of this study showed that coagulation bath temperature effect directly to the permeability of pure water and retention to sodium chloride rejection. The increasing of coagulation bath temperature resulted in higher permeability of membrane but lower rejection to sodium chloride while decreasing the coagulation bath temperature resulted in lower permeability of membrane but higher rejection to sodium chloride. The membrane prepared with coagulation bath temperature of 5°C shows the highest rejection for sodium chloride with 27 % of rejection. While for 27°C of coagulation bath managed to reject 22% of sodium chloride and the membrane prepared with coagulation bath temperature of 50°C only rejected 17% of the sodium chloride. The results obtained were coherent with the theory of the coagulation bath temperature effect even though fabricated under different conditions and materials.

ABSTRAK

Tujuan kajian ini dijalankan adalah untuk mengetahui kesan suhu larutan pengental kepada struktur dan pengaruh pemisahan membran terhadap larutan garam. Parameter ini penting untuk dikaji kerana suhu larutan pengental didapati bertindak secara terus kepada prestasi dan struktur membran. Dalam kajian ini membran kepingan rata daripada sistem ternari di sediakan melalui fasa basah balikan yang terdiri daripada polimer berkomposisi 21 % polietersulfona, 72% pelarut dari N-metil-2-pirolidon dan 7% air dan dihasilkan menggunakan mesin pengacuan elektrik semi-aoutomatik. Membran yang terhasil diuji dalam beberapa larutan pengental yang berlainan suhu iaitu 5°C, 27°C dan 50°C. Penilaian prestasi membran diuji dari segi ketelapan terhadap air tulen dan pemisahan kepada larutan garam berkepekatan 0.01 molar. Hasil kajian terhadap kesan suhu larutan pengental terhadap kecekapan membran mendapati, apabila suhu larutan pengental adalah tinggi, kadar ketelapan membran terhadap air adalah tinggi namun kecekapan pemisahan membran terhadap larutan natrium klorida adalah rendah. Kesan yang sebaliknya apabila suhu larutan pengental adalah rendah, dimana kadar ketelapan terhadap air adalah rendah namun dapat memisahkan larutan garam dengan tinggi. Daripada eksperimen yang dibuat, didapati membran yang dihasilkan daripada larutan pengental bersuhu 5°C menunjukkan pemisahan terhadap garam yang paling tinggi iaitu 27%, manakala membran yang dihasilkan dengan larutan pengental pada suhu 27°C dapat memisahkan 22% larutan garam dan membran yang dihasilkan pada suhu 50°C untuk larutan pengental hanya dapat memisahkan sebanyak 17% larutan air garam. Daripada hasil kajian yang diperolehi, didapati pengaruh suhu larutan pengental terhadap membran mempunyai persamaan dengan teori walaupun di hasilkan daripada bahan dan keadaan yang berbeza.